

# A NEW METHOD TO MEASURE FLARE COMBUSTION EFFICIENCY IN REAL-TIME

Presented by  
Yousheng Zeng, PhD, PE and Jon Morris  
*Providence*

at  
A&WMA Louisiana Section 2012 Fall Conference  
October 30-31, 2012

# INTRODUCTION



# 2010 TULSA FLARE STUDY

- Captured flare plume gases, analyzed composition, and determined Combustion Efficiency (CE) and Destruction and Removal Efficiency (DRE)
- Yielded important findings regarding steam and air assist and their impact on CE and DRE
- Demonstrated high variability in CE and DRE – potential benefits if CE could be monitored and fed back to operator in real time
- Extremely large effort; not suitable for routine monitoring



# FTIR-BASED HYPER-SPECTRAL IMAGER

- Advantages

- Imaging the flare plume (2-D compared to a path measurement; 3-D data cube)
- High spectral resolution

- Disadvantages

- Low frame rate (~1 scan/sec) – flare plume may have changed significantly during the same measurement cycle
- Specialist required for data reduction and analysis
- Not suitable for unmanned operations or long-term monitoring

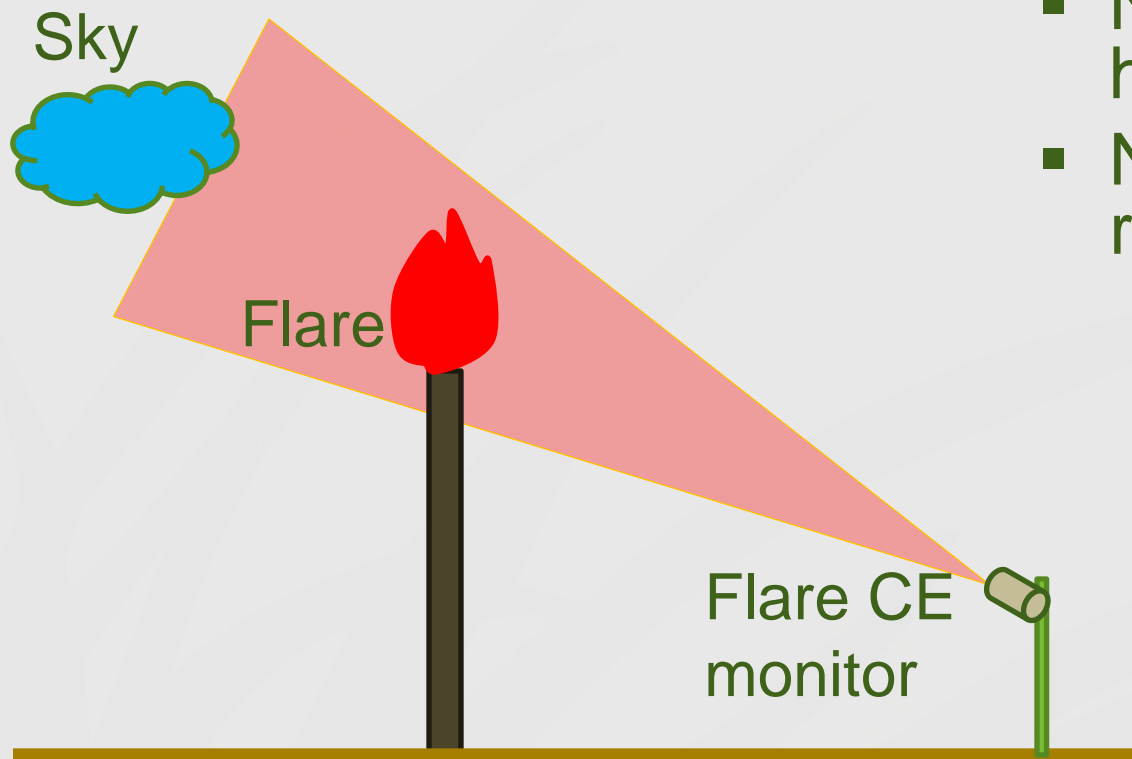
# PASSIVE FTIR

- Advantages
  - High spectral resolution
- Disadvantages
  - Path measurement – representativeness and aiming issues
  - Low scan rate with respect to the rate of change in flare plume
  - Specialist required for data reduction and analysis

# THE CONCEPT OF FLARE CE MONITOR

- Patented and patent-pending technologies using a 4-band MWIR imager that can
  - Image the flare plume, and
  - Measure flare CE at pixel level
  - Determine overall flare CE
- Major difference from FTIR based measurement – high frame rate: ~30Hz. As a result, temporal and spatial changes of flare plume within each CE measurement cycle become negligible
- Design objective: real time CE output suitable for integration into plant data systems for
  - Flare operators, or/and
  - Process control

# SETUP OF THE NEW FLARE CE MONITOR



- Not a path measurement
- No scanning; high frame rate
- No operator required

# THEORETICAL BASIS FOR THE NEW FLARE CE MONITOR





Typical Flare Combustion:

Fuel = hydrocarbon (HC); generically expressed as  $C_nH_y$



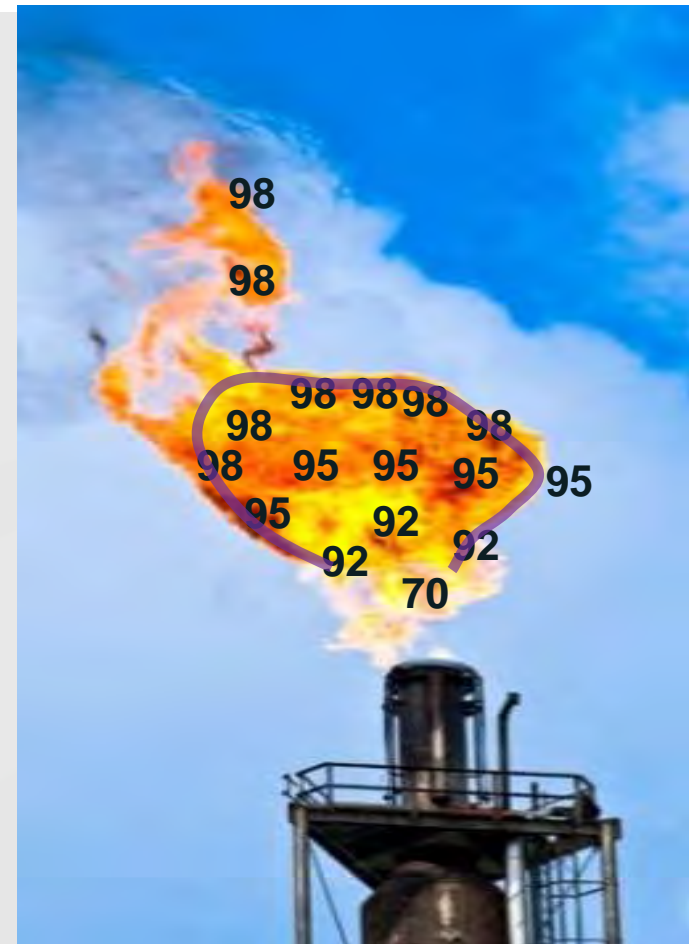
plus some CO if combustion is incomplete

Flare Combustion Efficiency (CE):

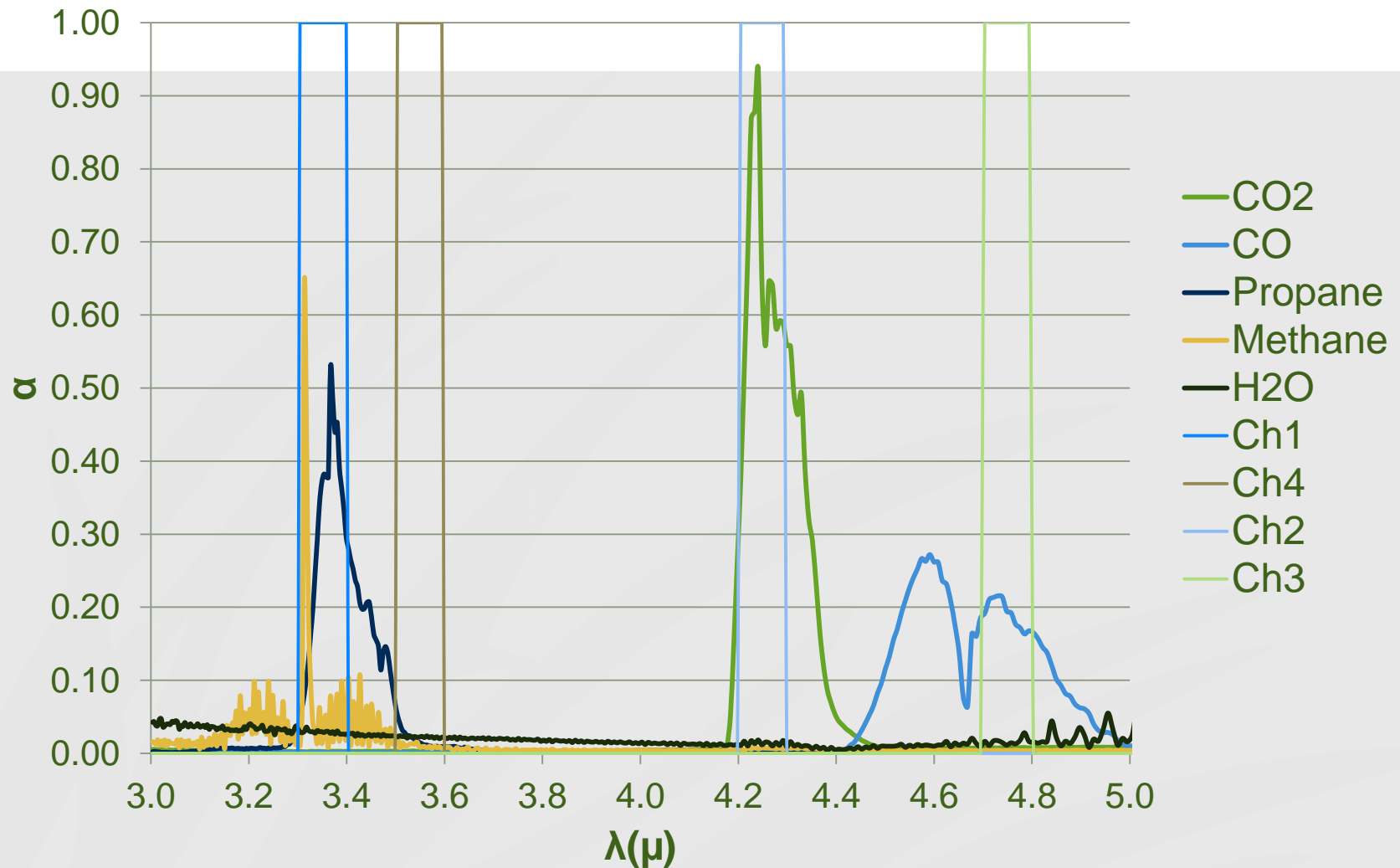
$$CE(\%) = \frac{[C]_{CO_2}}{\sum_i n_i [C]_{HC_i} + [C]_{CO_2} + [C]_{CO}} \quad \text{Eq. (1)}$$

# GENERAL IDEA

- Use a 4-band, high frame rate (~30 fps) Infrared (IR) imager to measure  $\text{CO}_2$ , CO, and HC and calculate CE
  - Band 1 (Ch1) for HC
  - Band 2 (Ch2) for  $\text{CO}_2$
  - Band 3 (Ch3) for CO
  - Band 4 (Ch4) for reference
- Each pixel in the image represents a region in the flare plume; CE measured at pixel level
- Relative strength of signals are measured per Eq. (1); calibrations are achieved through the Ref. Channel (Ch4)
- Overall CE is determined by averaging pixel level CE on pixels that form the flare plume “envelope” (pattern recognition algorithms are used to determine the envelope)



# SELECTION OF FOUR SPECTRAL BANDS



# SIMPLIFIED RADIATIVE TRANSFER EQUATION (RTE)

$$I = \varepsilon(\lambda)B(T_b, \lambda)\exp[-\alpha(\lambda)CL] + B(T_g, \lambda) - B(T_g, \lambda)\exp[-\alpha(\lambda)CL]$$

$$B(T, \lambda) = \frac{2hc^2}{\lambda^5} \frac{1}{e^{\frac{hc}{\lambda k_B T}} - 1}$$

When  $T_g \gg T_b$ ,

$$I \approx B(T_g, \lambda) - B(T_g, \lambda)\exp[-\alpha(\lambda)CL]$$

Taylor Expansion:  $e^x = 1 + \frac{x}{1!} + \frac{x^2}{2!} + \frac{x^3}{3!} + \dots$ ,  $-\infty < x < \infty$

When  $x \ll 1$ ,  $e^x = 1 + x$

$$I \approx B(T_g, \lambda) - B(T_g, \lambda)[1 - \alpha(\lambda)CL] = B(T_g, \lambda)\alpha(\lambda)CL$$

$$C = \frac{I}{B(T_g, \lambda)\alpha(\lambda)L} \quad \text{Eq. (2)}$$

# EQUATION FOR FLARE CE MEASUREMENT

- Substitute C in Eq. (1) with Eq. (2);
- Use subscripts 1, 2, 3 for HC (Channel 1), CO<sub>2</sub> (Channel 2), and CO (Channel 3), respectively;
- Cancel out L; and
- Use weighted avg. n and α for HC.

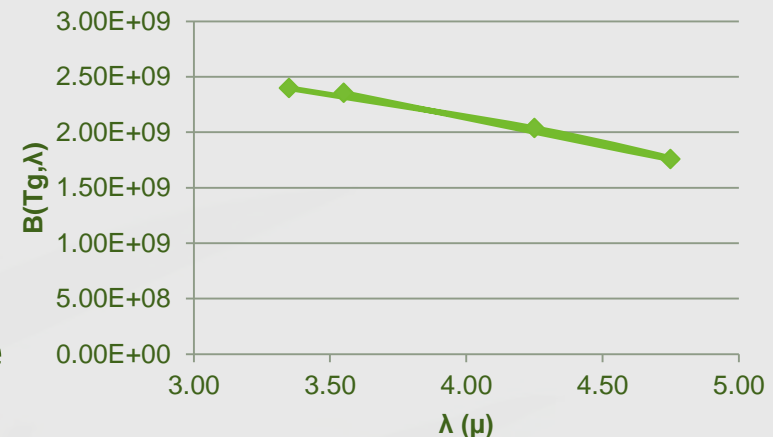
Eq. (2) becomes:

$$CE (\%) = \frac{\frac{I_2}{B(T_g, \lambda_2) \alpha(\lambda_2)}}{\bar{n} \frac{I_1}{B(T_g, \lambda_1) \bar{\alpha}(\lambda_2)} + \frac{I_2}{B(T_g, \lambda_2) \alpha(\lambda_2)} + \frac{I_3}{B(T_g, \lambda_3) \alpha(\lambda_3)}} \quad \text{Eq. (3)}$$

# VARIOUS MEASUREMENT APPROACHES CONSIDERED

$$CE(\%) = \frac{\frac{I_2}{B(T_g, \lambda_2)\alpha(\lambda_2)}}{\bar{n} \frac{I_1}{B(T_g, \lambda_1)\bar{\alpha}(\lambda_2)} + \frac{I_2}{B(T_g, \lambda_2)\alpha(\lambda_2)} + \frac{I_3}{B(T_g, \lambda_3)\alpha(\lambda_3)}} \quad \text{Eq. (3)}$$

- $B(T_g, \lambda_i)$ :
  - Method 1 – Assume the 4  $\lambda$ 's are close enough and  $B(T_g, \lambda)$  for the three channels are equal (and cancelled out)
  - Method 2 – Use the Ref. Band (Ch4) and Planks law to determine  $T_g$  and calculate  $B(T_g, \lambda_i)$  for other 3 channels – Not desirable and not used at this time
  - Method 3 – Calculate ratios of  $B(T_g, \lambda_i)/B(T_g, \lambda_{\text{Ref}})$  in the expected temp. range (e.g., 800-1200 °F)



# VARIOUS MEASUREMENT APPROACHES CONSIDERED

$$CE (\%) = \frac{\frac{I_2}{B(T_g, \lambda_2) \alpha(\lambda_2)}}{\bar{n} \frac{I_1}{B(T_g, \lambda_1) \bar{\alpha}(\lambda_2)} + \frac{I_2}{B(T_g, \lambda_2) \alpha(\lambda_2)} + \frac{I_3}{B(T_g, \lambda_3) \alpha(\lambda_3)}} \quad \text{Eq. (3)}$$

- $\alpha(\lambda_i)$ :
  - For  $\text{CO}_2$  and  $\text{CO}$ , values of  $\alpha(\lambda)$  are calculated based on their IR spectra
  - For HC, use weighted avg. (need some knowledge of flare gas composition)
  - Correction for  $\text{H}_2\text{O}$  – see next slide

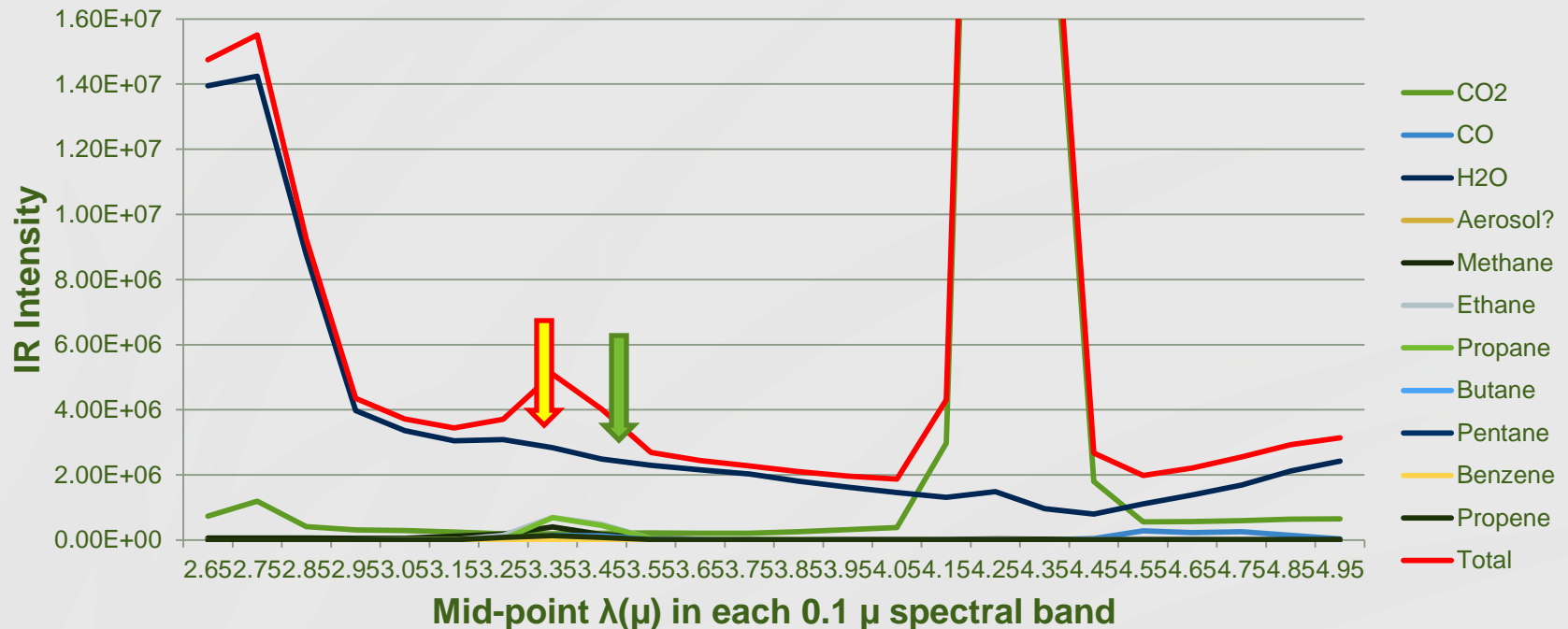
# EFFECT OF GAS PHASE H<sub>2</sub>O

- Correction factor =  $\frac{\alpha(\lambda_1)}{\alpha(\lambda_4)}$  Independent of H<sub>2</sub>O conc.!

Where  $\alpha(\lambda)$  = absorption coefficient of H<sub>2</sub>O at wavelength of Ch1 and Ch4

$$\frac{I_1}{I_4} = \frac{B(T_g, \lambda_1) \alpha(\lambda_1) C_{H_2O} L}{B(T_g, \lambda_4) \alpha(\lambda_4) C_{H_2O} L}$$

$$\frac{I_1}{I_4} = \left[ \frac{B(T_g, \lambda_1)}{B(T_g, \lambda_4)} \right] \left[ \frac{\alpha(\lambda_1)}{\alpha(\lambda_4)} \right]$$





# SIMULATION RESULTS



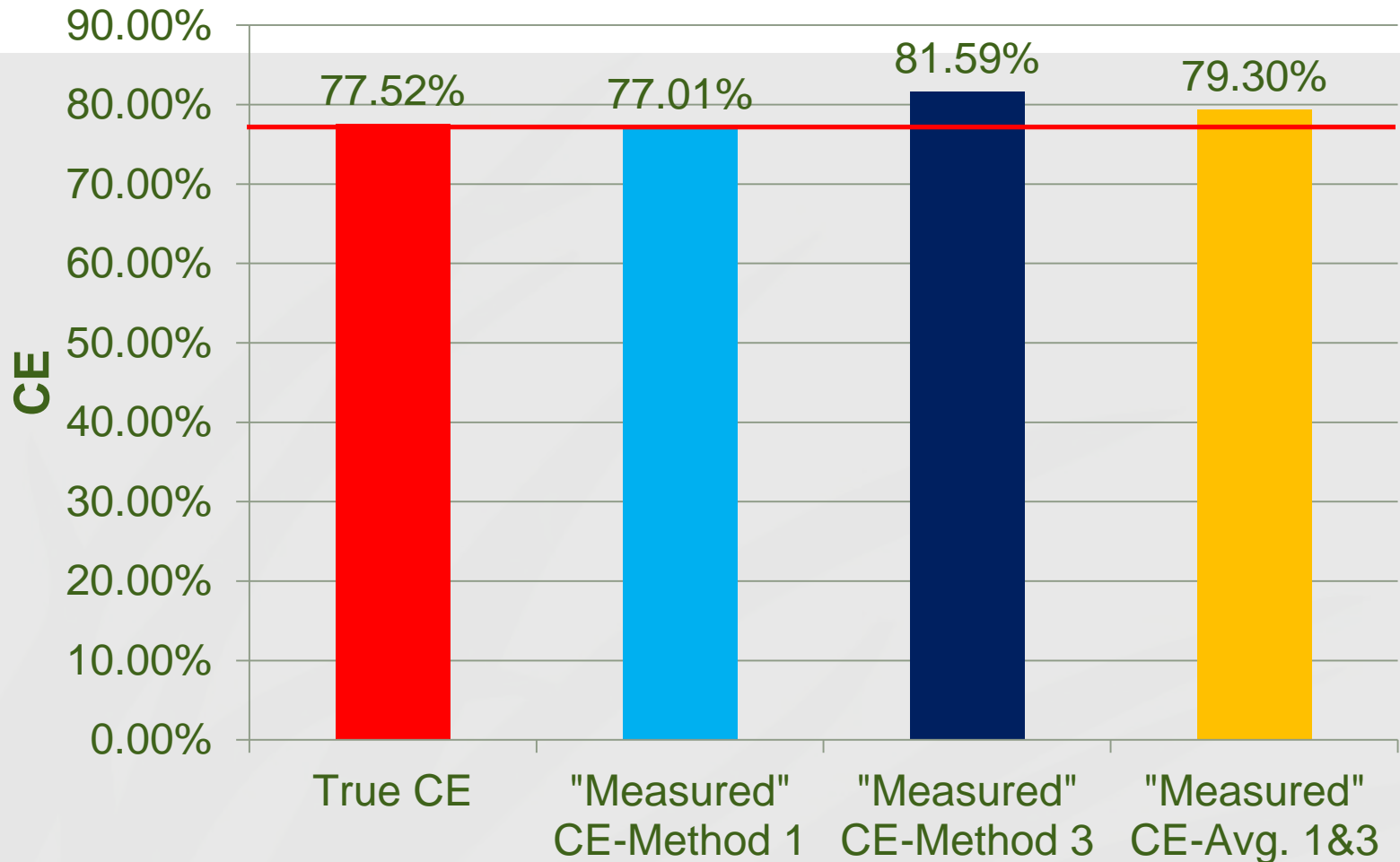
# SIMULATED FLARE PLUME

- Flare gases: typical refinery fuel gas (ref. John Zink Combustion Handbook)
- Assumptions for Base Case (Case 1):
  - Plume temp=800 F
  - Plume depth=1 m (3.28 ft.)
  - Distance from flare to the CE monitor=300 ft.

Assumed Composition  
in flare plume

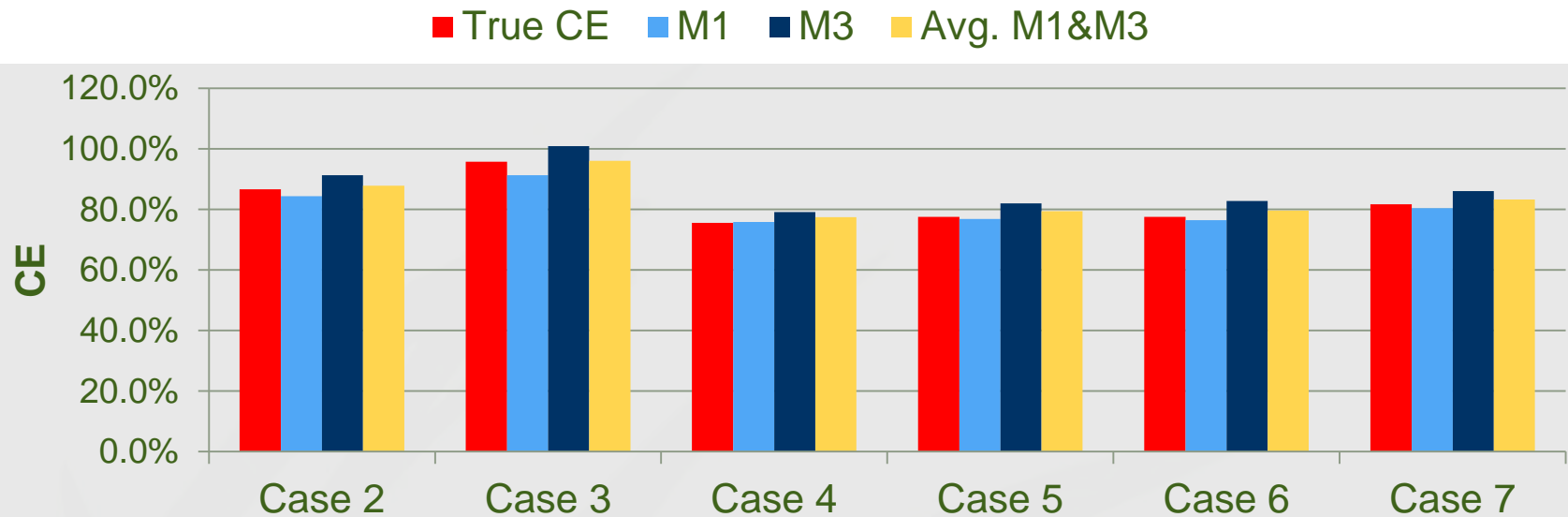
Compound	Conc.
CO <sub>2</sub>	12.000%
CO	0.200%
H <sub>2</sub> O	15.960%
Methane	0.720%
Ethane	0.360%
Propane	0.400%
Butane	0.040%
Pentane	0.000%
Benzene	0.000%
Propene	0.160%

# SIMULATED RESULT – BASE CASE (CASE 1)



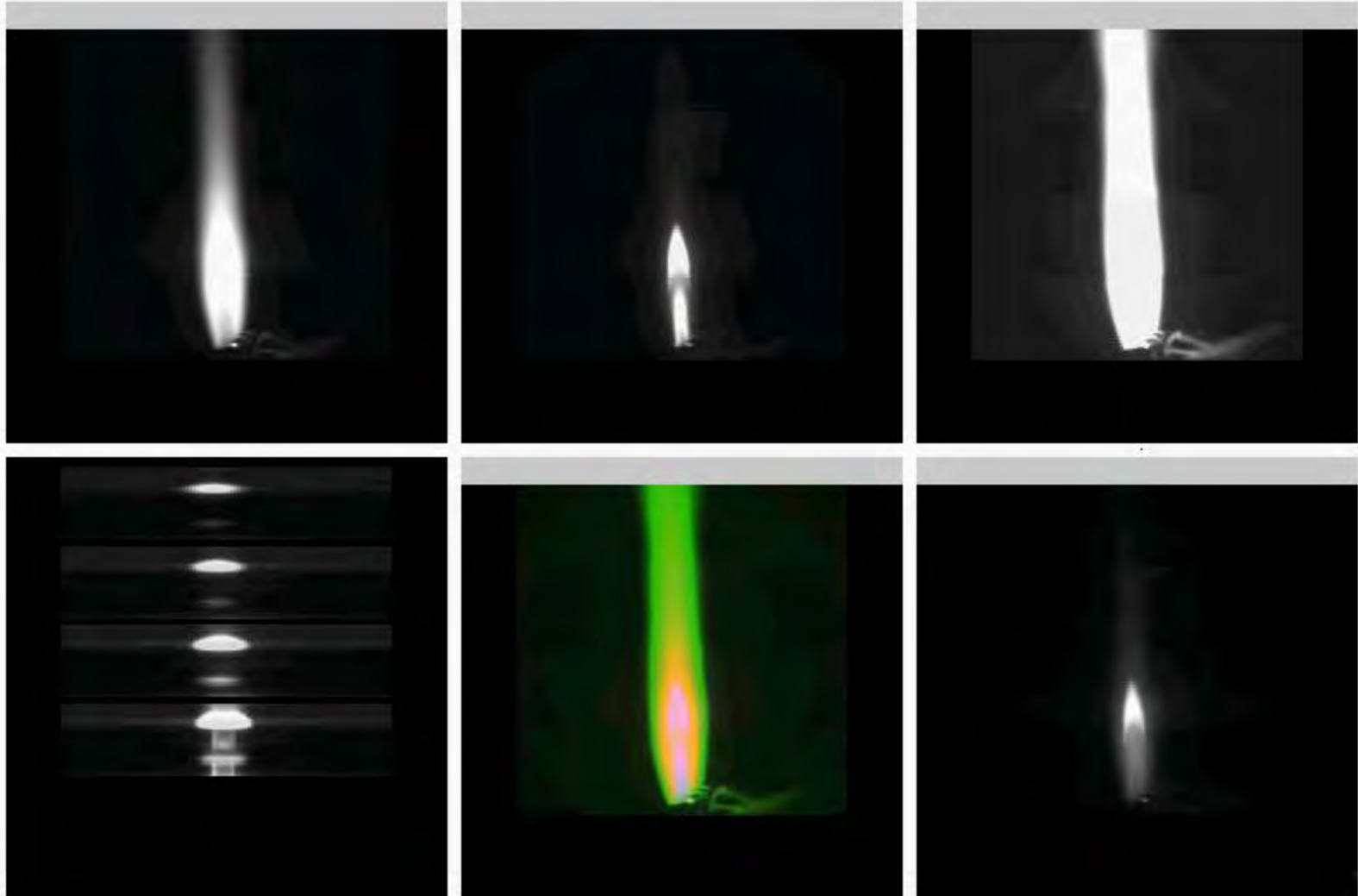
# SIMULATED RESULTS – CASES 2-7

## EFFECT OF FLARE GAS COMPOSITION AND H<sub>2</sub>O



- Case 2: Unburned fuel=1/2 of Case 1
- Case 3: Unburned fuel=1/10 of Case 1
- Case 4: Double the conc. of ethane and add pentane and benzene
- Case 5: Add 10% more H<sub>2</sub>O in the plume
- Case 6: Add 30% more H<sub>2</sub>O in the plume
- Case 7: Add 30% more CO<sub>2</sub> in the plume

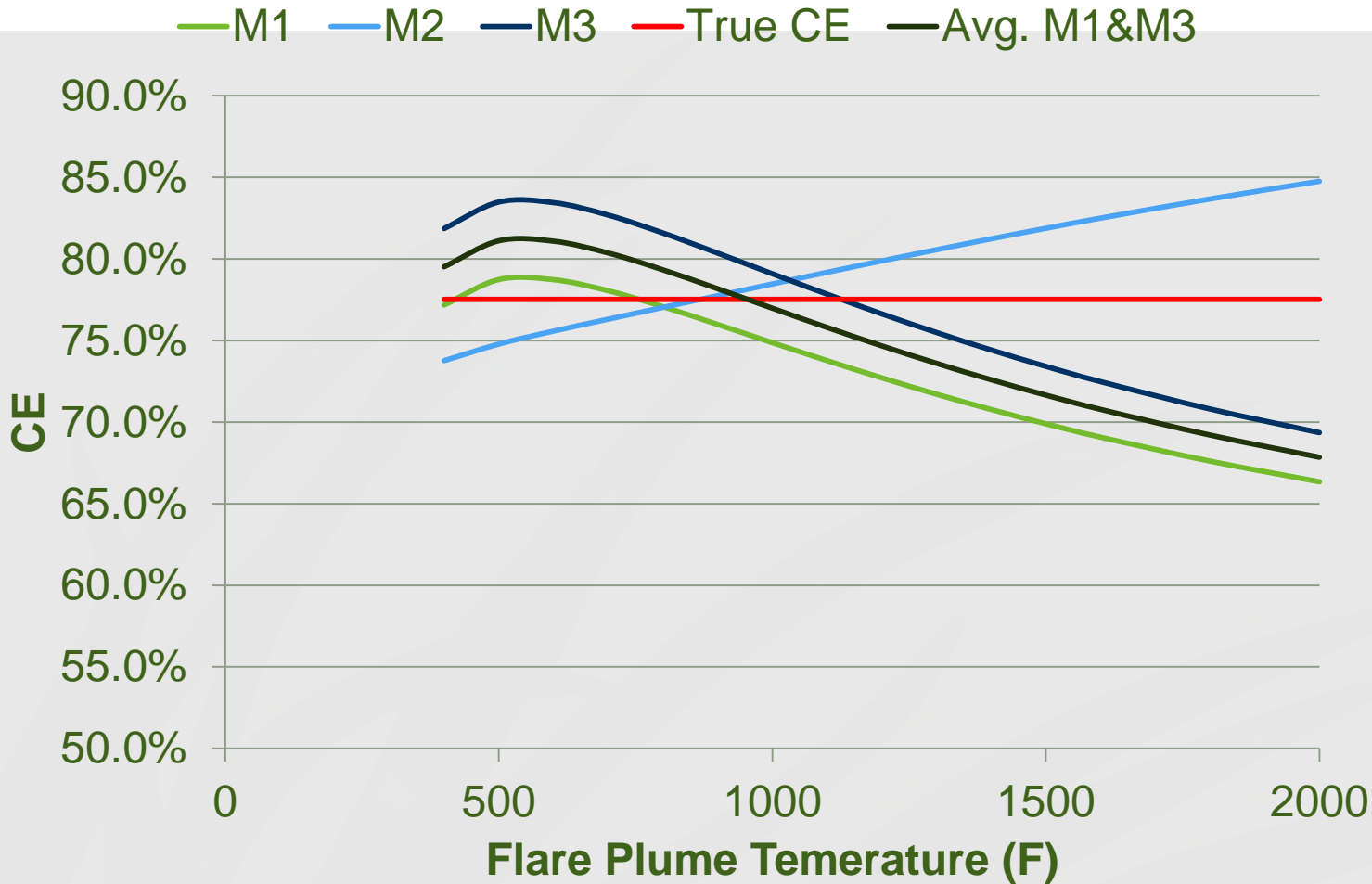
# A SIMPLE EXPERIMENT USING A BUTANE BURNER AND LAB MULTI-SPECTRAL IR IMAGER



# A SIMPLE FIELD EXPERIMENT USING 2 SPECTRAL BANDS

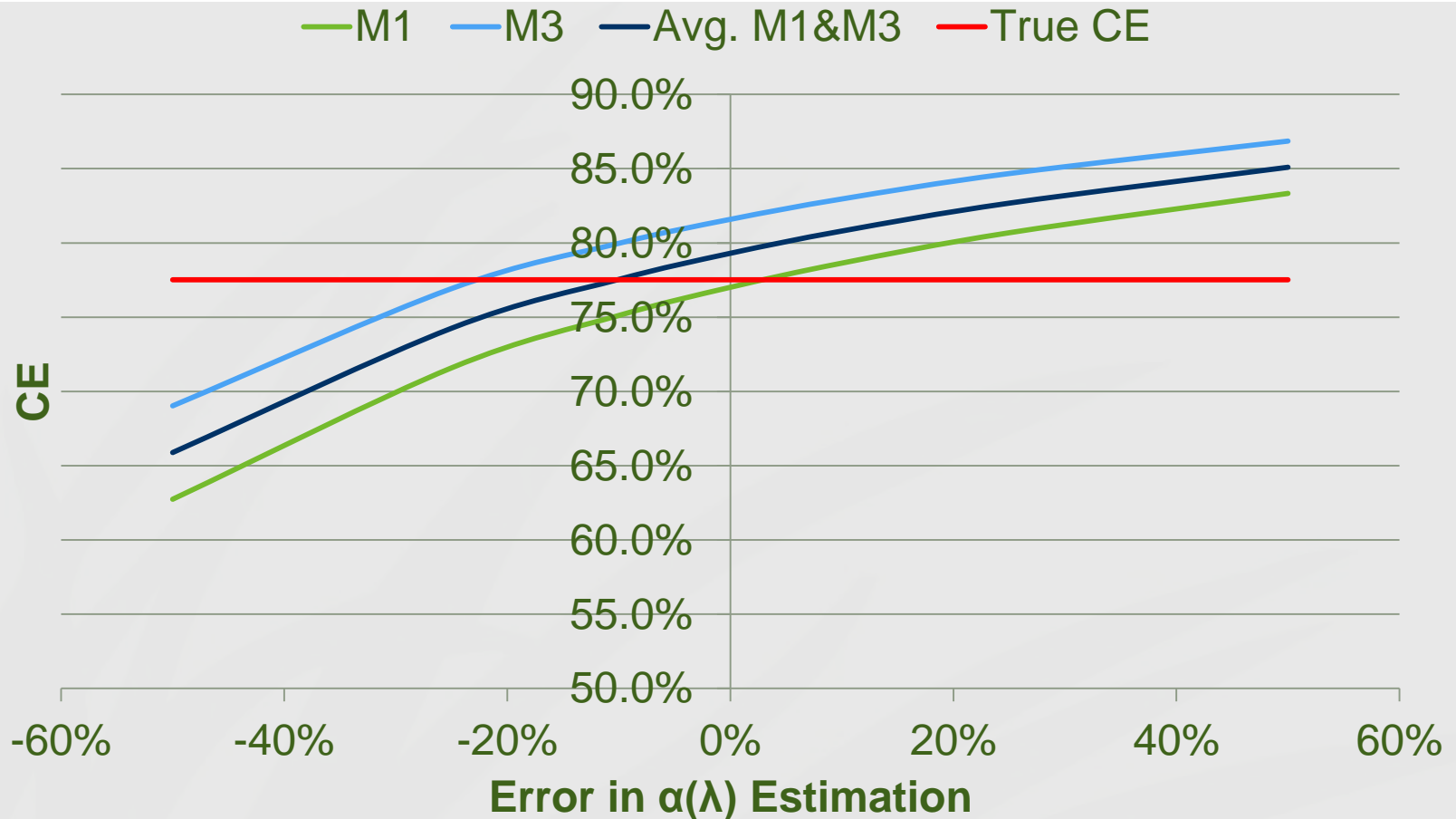
- Dual cooled Mid-Wave IR cameras with different spectral filtering (i.e., 2 of the 4 bands required for CE monitor)
- Emission plume with steam and propane thoroughly mixed
- Steam emission rate: 1200 lb/hr
- Propane emission rate: 3 lb/hr
- Plume diameter at release: 3 inches
- Distance from cameras: 175 feet
- Demonstrated the ability to identify and isolate propane from steam at the pixel level using spectral radiance

# EFFECT OF PLUME TEMPERATURE



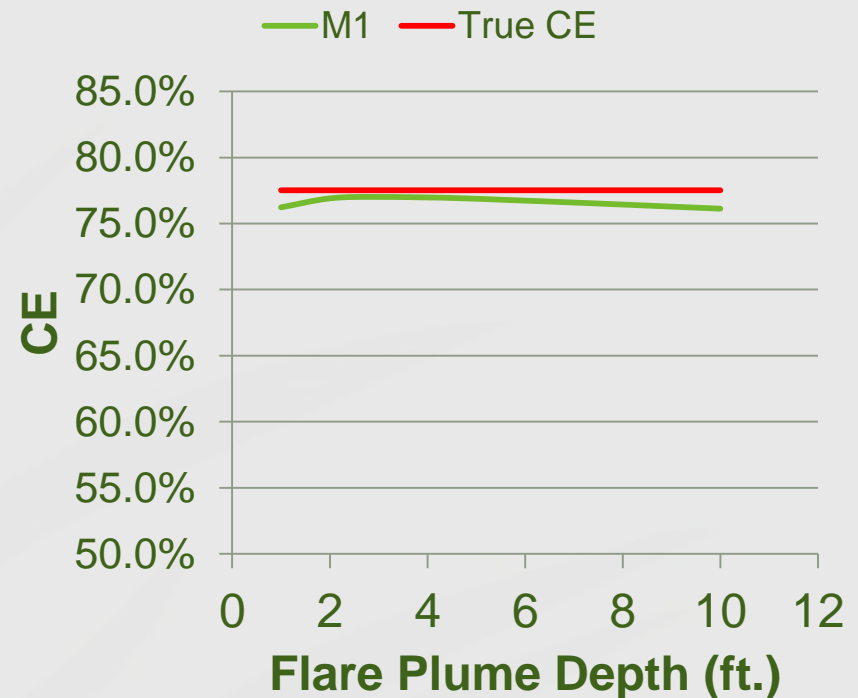
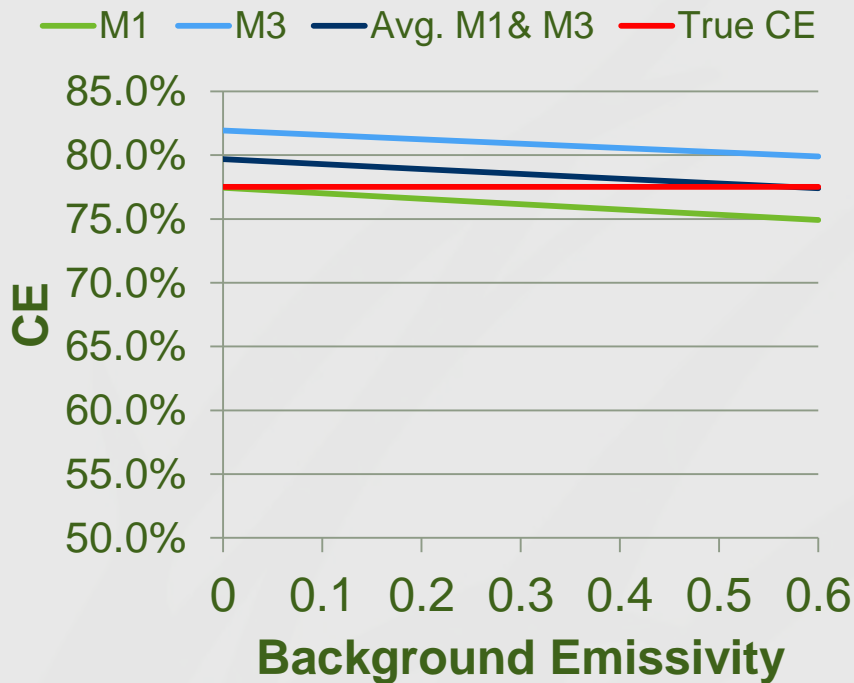
Note:  
pixels are  
expected  
to cover  
flare's  
high and  
low T  
regions

# EFFECT OF ERROR IN HC ABSORPTION COEFFICIENT ESTIMATION





# EFFECT OF BACKGROUND EMISSIVITY AND FLARE PLUME DEPTH



# CONCLUSION



# CONCLUSION

- Theoretical analysis and model simulation results demonstrate the feasibility of the real-time flare CE monitoring device
  - Influential factors: plume temperature, estimate of HC absorption coefficients based on knowledge of flare gas composition
  - Less significant factors: plume depth, background, flare gas composition, actual CE
  - Calibration is accomplished inherently through the Reference Channel in the CE calculation which relies on *relative* measurements at the pixel level; no external calibration is required
- Field experiment with propane and steam demonstrates the feasibility of cancelling out interferences by using two spectral bands

# NEXT STEPS

- Perform field experiment using a 42-band laboratory spectral imager to further prove the concept and narrow the design parameters
- Design and develop the first prototype
- Extensive field testing
- Launch commercial product